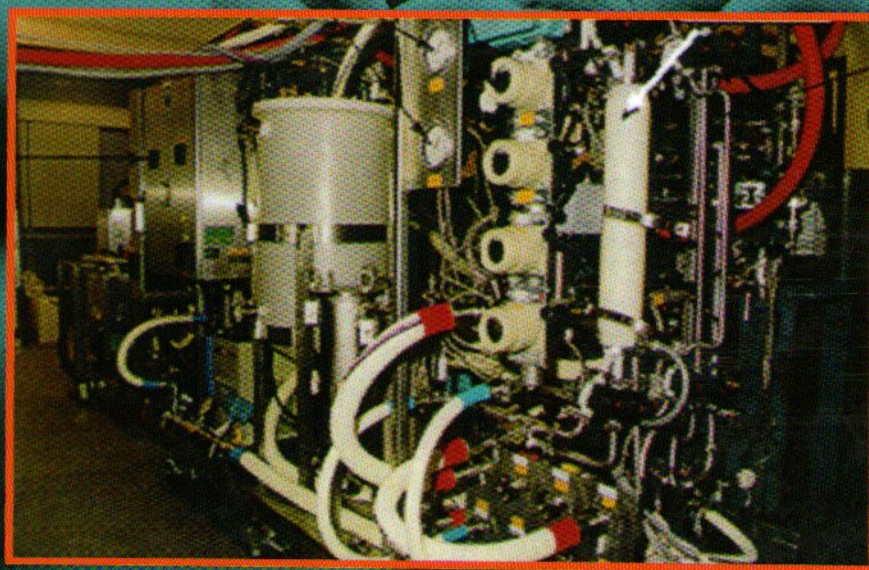


SECOND EDITION

# *Handbook of* **Membrane Separations**

**Chemical, Pharmaceutical, Food,  
and Biotechnological Applications**



Edited by

**Anil K. Pabby**

**Syed S.H. Rizvi**

**Ana Maria Sastre**

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# Advanced materials for ultrafiltration and nanofiltration membranes

W.J. Lau, A.F. Ismail, T. Matsuura, N.A. Nazri, E. Yuliwati

<sup>a</sup>Advanced Membrane Technology Research Centre (AMTEC),

<sup>b</sup>Faculty of Petroleum and Renewable Energy Engineering,  
Universiti Teknologi Malaysia, 81310 UTM, Skudai Johor, Malaysia  
Tel. +60 (7) 553-5592; Fax: +60 (7) 558-1463

<sup>c</sup>Faculty of Industrial Engineering,  
Universitas Bina Darma, 30251 Palembang, Indonesia,  
Tel. +62 (711) 515-679; Fax: +62 (711) 518-000

\*Corresponding author: [afauzi@utm.my](mailto:afauzi@utm.my)

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## 1. INTRODUCTION TO MEMBRANE-BASED LIQUID SEPARATION PROCESSES

Membrane separation technologies refer to any separation processes in which membrane function as both a barrier and a sieve for separating feed species such as liquid mixtures and colloidal particle mixtures [1-3]. Compared with conventional separation methods, membrane separation technologies have the following advantages, (i) *Efficient*, Generally, a membrane separates feed species in combination of sieving effect and affinity effect. The development in material science helps readily the membrane separation of most difficult mixtures; (ii) *Energy saving and environment protective*, Size-based separation processes such as ultrafiltration (UF),

nanofiltration (NF) and reverse osmosis(RO), involve without heat induced phase transition and require much energy loss consumption. Moreover, a considerable portion of membrane separation technologies play important roles in environmental issues such as water treatment, pollutant processing, and hazardous organics recovery; (iii) *Versatile*, the application scope of membrane separation technologies is broad and flexible, benefiting both the industry and daily lives.

Membrane science can arbitrarily be divided into seven intimately related categories: material selection, material characterization and evaluation, membrane preparation, membrane characterization and evaluation, transport phenomena, membrane module design, and process performance. Among these categories, membrane materials are currently the most important part in membrane technology and it was experiencing significant growth. These materials differ in their performance characteristics including mechanical strength, fouling resistance, hydrophobicity, hydrophilicity, and chemical tolerance. Moreover, materials capable of performing multiple functions simultaneously or sequentially in time are of significance to improve performance of membranes.

For water treatment, hydrophobicity and hydrophilicity play very important role. Hydrophilic means water-loving and such materials readily adsorb water. The surface chemistry allows these materials to be wetted forming a water film or coating on their surface. Hydrophobic means water-hating and this materials has little or no tendency to adsorb water. Water tends to bead on hydrophobic surfaces into discrete droplets. The hydrophilic and hydrophobic properties of a membrane material are related to the surface tension of the material. The fundamental importance of the surface tension comparison is that liquids having lower surface tension values will generally spread on materials of higher surface tension values. Table 1 summarizes surface tension values of some polymeric membrane materials. It has been noted that the higher of surface tension value of material, the more hydrophilic the material is.

**Table 1.**  
**Summarized surface tension of some polymeric materials [4].**

Polymer materials	Surface tension (dynes/cm)
Polytetrafluoroethylene	18
Polyvinylidene fluoride	25
Polypropylene	29
Poly vinyl chloride	39
Polysulfone	41
Polycarbonate	42
Polyacrylonitrile	44
Cellulose	44

Hydrophilic membranes tend to exhibit greater fouling resistance than hydrophobic membranes. Particles that foul in aqueous media tend to be hydrophobic. Hydrophobic particles tend to cluster or group together to form colloidal particles because this lowers the interfacial free energy (surface tension) due to the surface area exposure. To prevent fouling in water or

wastewater treatment, a membrane requires a surface chemistry, which prefers binding to water over the other materials.

## **2. RECENT DEVELOPMENT IN MEMBRANE MATERIALS**

Significant progress has been made during recent years in the development of new membranes and their applications. This development of a certain membrane process or application can be classified according to the driving force used in the process. The technically and commercially most relevant processes are pressure-driven processes, such as reverse osmosis, ultrafiltration and nanofiltration. In this chapter the principles of relevant membrane materials are briefly reviewed. An assessment of the present and future membrane materials is given. The structure of the membrane-based industry and its strategies toward the application and market are slightly described. Recent developments of new or improved membranes are discussed and further research needs for a continuous growth of membrane technology are pointed out.

Membrane materials are core parts of any membrane-based technologies [5-7]. In the past decades, the conception of multi-component or composite membrane materials has been a successful methodology for designing membrane materials with optimum performances. This is because single component materials, no matter natural or synthesized, can hardly fulfill all of the requirements for making an ideal separation membrane. On the other hand, multi component composite materials can combine advantages of different components and achieve optimum properties and performances.

Numerous interesting scientific and technological challenges are presented by the area of polymer-based membrane materials which are used for materials separation and catalysis [8-11]. The balance between the permeability and flux of a membrane material with respect to specific compositions of the liquids to be separated in specific applications with substantial market potential, such as drinking water process, require an extremely high degree of optimization, which is frequently not attainable with traditional homopolymers. For this reason, multicomponent polymers are also being developed. There is little known to date concerning the relationships between the topologies and properties of these polymers. The stabilization of the structure of polymers with intrinsic microporosity, which could be used for applications in the field of water separation, and also demonstrate particularly interesting properties in the separation of liquid material mixtures, offers another challenge.

### **2.1 ULTRAFILTRATION**

Ultrafiltration (UF) has become one of the best alternatives replacing conventional liquid separation process. However, membrane fouling is a critical issue in UF process and also an important factor, which restrict its widespread application. Development of new materials is accompanied by developments in process engineering aimed at optimizing the design of separation processes.

The activities in this area are divided into two groups: polymer multicomponent and organic-inorganic hybrid materials. Due to the distinct advantages such as temperature and wear

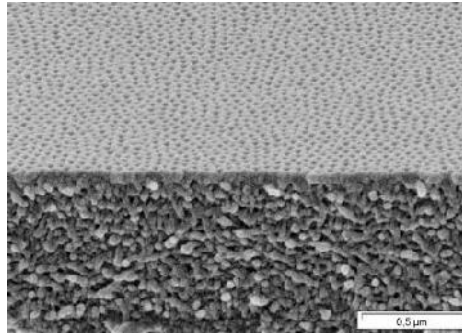
resistance, well defined stable pore structure, and chemical inertness, the inorganic membranes such as ceramic and carbon membranes are quite suitable for the processes involving high temperatures and harsh chemical environments and have been successfully applied to the water or wastewater treatment [12-14]. However, inorganic membranes display some inherent disadvantages and majority of them are related to their relatively high cost arising from the expensive materials, the complicated fabrication procedure and the low membrane surface [15]. Hence, the cheap and easy-fabricating polymeric membranes are still dominating the membrane market. It should be pointed out that the serious membrane fouling caused by nonspecific adsorption and/or deposition of foulant onto membrane surfaces, often results in a substantial decline of the permeate flux with operation time and consequently limits their wide application in the water and wastewater treatment [16]. Many investigations have demonstrated that modifying membrane surface, such as hydrophilicity, pore size, porosity and surface charge effectively inhibited the nonspecific adsorption and consequently decreases membrane fouling and increases significantly the permeate flux [17-19]. The improvement of polymer/polymer and polymer/inorganic blend membranes are most interesting, owing to its convenient operation under mild conditions and good performances of the resulting membranes.

### **2.1.1 Polymer/Polymer Blend Membranes (Polymer Multicomponent Systems)**

The molecular self-organization of block copolymers with different topologies presents a remarkably fascinating strategy for the formation of nanostructured membrane materials. Molecular self-organization is the spontaneous arrangement of molecules in highly-ordered structures held together by intermolecular bonds. Although synthetic membranes are much more simply structured and demonstrate much lower degrees of functionality than biological membranes, their mechanisms of structural formation are nonetheless very similar. To this end, tailor-made block copolymers of differing chemical composition are synthesized, using controlled polymerization processes, and morphologically characterized. During this process, additional functionality can be provided by integrating stimuli-sensitive blocks, which results in switchable membranes. The process of structural formation during membrane production also plays a substantial role here. Also studied, in addition to pure block copolymers, are mixtures of various polymers, which are normally available commercially.

#### **2.1.1.1 Integral-asymmetrical block copolymer membrane**

The molecular self-organization of block copolymers with different topologies presents a remarkably fascinating strategy for the formation of nanostructured membrane materials, as shown in Figure 1 [20]. Molecular self-organization is the spontaneous arrangement of molecules in highly-ordered structures held together by intermolecular bonds. Although synthetic membranes are much more simply structured and demonstrate much lower degrees of functionality than biological membranes, their mechanisms of structural formation are nonetheless very similar.



**FIGURE 1** Integral-asymmetrical block copolymer membrane

To this end, tailor-made block copolymers of differing chemical composition are synthesized, using controlled polymerization processes, and morphologically characterized. During this process, additional functionality can be provided by integrating stimuli-sensitive blocks, which results in switchable membranes. The process of structural formation during membrane production also plays a substantial role here.

Also studied, in addition to pure block copolymers, are mixtures of various polymers, which are normally available commercially. All these systems should incorporate at least one semipermeable component, while other insoluble and non-swellable components serve to stabilize the membrane.

**Table 2**  
**Polymer/polymer blended membranes**

Polymer used	Method	Remark	Reference
PES/PVP	Diffusion induced phase separation with acrylonitrile-based copolymer		[21]
SPC/PVDF	Sulfonation of polycarbonate blended to PVDF	The blend of two different polymers showed the slow low flux declinations, low fouling due to electric exclusion.	[22]
PS/PMMA	Direct blended	The polar group in PS enhanced miscibility in blend containing PMMA	[23]
PVDF/PC	Direct blended using PMMA as compatibilizer	This membrane demonstrated that 40% of PMMA generates	[24]

			an increase in miscibility and a beneficial effect on permeability.	
PEI/SPEI	Direct blended		These SPEI/PEI membranes showed anti-fouling properties regarding BSA flux at pH 8, achieving 32% reduction as compared to 75% PEI.	[25]
PVDF/PFSA	Direct blended		The anti-fouling property of PVDF-PFSA-H membrane was superior to PVDF-PFSA-Na	[26]
PVDF/PMMA	Direct blended		The good blending of both polymers is due to the presence of basic oxygen in PMMA and an acidic hydrogens in PVDF, thus enabling H-bond interactions. These membrane resulted lower fouling and enhanced permeate quality with lower COD as compared to a PVDF membrane.	[27]
PEI/SPEEK	Direct blended		The hydraulic permeability ( $L_h$ ) increased from $24 \times 10^{-11}$ to $36 \times 10^{-11} \text{m}^3 \text{s}^{-1} \text{N}^{-1}$ .	[28]
CA/SPES	Direct blend membrane	UF	This group achieved membranes presenting a 29-69 kDa MWCO and an increase in hydraulic permeability.	[29]

In summary, the blend of two different polymers confers important characteristics such as structure alteration and antifouling properties to UF membrane. The interest of these studies is to generate membranes, that in addition to separate emulsion by size exclusion. Moreover, this showed also the low flux decline, low fouling due to electric exclusion by means of having surface and pore charge of the same sign as emulsion charge.

### 2.1.2 Polymer/Inorganic Composite Membrane

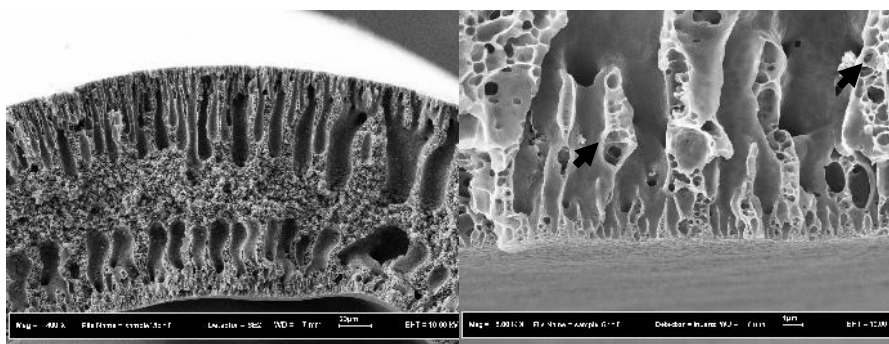
The dispersion of inorganic particles in the polymer matrix have been useful in the improvement of membrane performance. The preparation of membranes formed by inorganic particles uniformly dispersed in a polymer matrix has received much attention from several years. There

are many inorganic nano-particles which have been used to prepare polymeric membrane such as  $\text{TiO}_2$ ,  $\text{SiO}_2$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{Fe}_2\text{O}_3$ , and  $\text{ZnO}$ [30,31]. Beneficial effects of certain types of nanoparticles on membrane modification have been reported, such as the amelioration of surface hydrophilicity and enhancement of antifouling property [32-34].

### 2.1.2.1 Polymer membrane with addition of titanium dioxide ( $\text{TiO}_2$ )

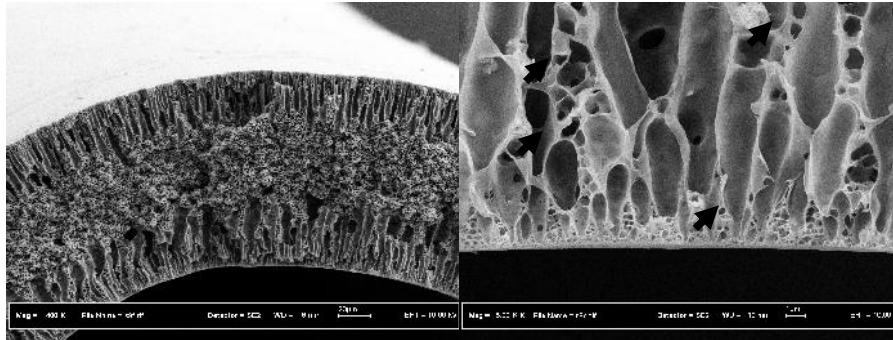
In recent years,  $\text{TiO}_2$  nanoparticles have been commonly used to degrade contaminants in water treatment processes [35]. Several studies have demonstrated that the  $\text{TiO}_2$ -doped membranes [36-38]. Wei et al. [39] prepared the modified PVDF membranes by adding different amounts of  $\text{TiO}_2$  nanowire into the casting solution, and investigated their bacterial, photocatalytic and anti fouling properties. Results showed that  $\text{TiO}_2$  particles addition significantly affected the pore size and hydrophilicity of the membrane and thus improved the flux and permeability of the modified PVDF/ $\text{TiO}_2$  membrane.  $\text{TiO}_2$ -doped PVDF membrane also showed better bactericidal and antifouling abilities under UV light exposure compared with the neat PVDF membrane.

The effect of membrane characterization parameters on permeability and rejection was also investigated using submerged UF experiments by Yuliwati et al. [36]. As shown in Figure 2, PVDF with addition of 1.95 wt.%  $\text{TiO}_2$  (PTL-10) and 2.85 wt.%  $\text{TiO}_2$  (PTL-15) showed fluxes of  $146 \text{ L/m}^2 \text{ h}$  and  $82.97 \text{ L/m}^2 \text{ h}$ , respectively. The rejection values demonstrated the similar trend to the flux, showing the maximum value of 98.8 % at 1.95 wt.%  $\text{TiO}_2$  concentration (PTL-10). It is interesting to note that the observed trend is contrary to the trade-off effect, by which rejection should decrease as flux increases. It is easy to understand that the flux shows a maximum value for the membrane PTL-10, since both porosity and pore size become the highest for this particular membrane [36]. The maximum in rejection occurring at the same  $\text{TiO}_2$  concentration, on the other hand, can be explained by the trend observed in the surface hydrophilicity. Most likely, water is preferentially transported through the membrane as compared to the hydrophobic components of the refinery waste water when the membrane surface is hydrophilic, thus the highest rejection of oily components corresponds to the highest surface hydrophilicity of the membrane.



(a)





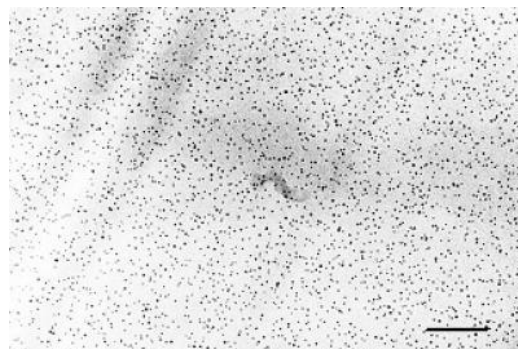
(b)

**FIGURE 2** The cross-sectional and outer surface images of hollow fibers (Mag. 800x) (a) PTL-10 and (b) PTL-15

TiO<sub>2</sub> particles on the membrane surface reduced the interaction between contaminants and the membrane surface. The increased membrane hydrophilicity and membrane pore size with lower TiO<sub>2</sub> concentration ( 1.95 wt.%) could attract water molecules inside the composite membrane; facilitated their penetration through the membrane, enhancing the flux and rejection. However, higher TiO<sub>2</sub> concentration (> 1.95 wt.%) resulted in the formation of a highly viscous dope.

### 2.1.2.2 Polymer membrane with addition of silver nanoparticles

Silver has been known to be a bactericide since ancient times. Recently, nanosized silver nanoparticles have been reported to exhibit antimicrobial properties [40]. The incorporation of Ag nanoparticles into various matrices has been intensively investigated to extend their utility in materials and biomedical applications [41,42]. Xue et al. [43] reported antimicrobial Ag nanoparticles immobilized on textile. Antibacterial test showed that the as-fabricated textiles had high antibacterial activity against the gram-negative bacteria, *Escheria coli*.



**FIGURE 2.5** Polymer membrane with silver nanoparticles

### **2.1.2.3 Polymer membrane with addition of zinc-oxide nanoparticles**

Zinc oxide (ZnO), with the completely hydrophilicity, is one of the most common raw materials in industry and suitable to be used to improve the hydrophilicity of the membrane. Furthermore, nanosized ZnO possesses not only the anti bacterial nature but also the valuable ultraviolet resistant property [44,45], which might potentially benefit the antifouling performance and extend the service life and application field of membranes. Moreover, nano-ZnO is much cheaper than TiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub> (Alumina) nanoparticles (1/4 price according to the Chinese market quotes). However, the related application of nano-ZnO for membrane modification has not been reported.

Liang et al. studied a novel anti-irreversible fouling PVDF membrane with addition of nano-ZnO as an additive, was successfully fabricated using non-solvent induced phase separation (NIPS) method [31]. The modification of internal surface of membrane pores was primarily concerned. Different dosage of nano-ZnO ranging from 6.7% to 26.7% (percentage of PVDF weight) was adopted for membrane modification. The filter ability and anti-irreversible fouling property of the resultant membranes were evaluated through testing water permeability, flux recovery and long-term filtration performance by dead-end filtration system. The sample membrane disk was precisely installed in a stirred dead-end cell (Amicon 8400, USA) with an effective membrane area of 41.8 cm<sup>2</sup> and constant stirring speed of 200 rpm at room temperature. All the modified membranes achieved almost 100% water flux recovery after physical cleaning, whereas the raw membrane only reached 78% recovery. The water permeability of the modified membrane almost doubled by adding 6.7% nano-ZnO which was determined as the optimum dosage for PVDF membrane modification. Additionally, the mechanical strength of was found reinforced for modified membrane.

### **2.1.2.4 Polymer membrane with addition of silica nanoparticles**

The addition of fine silica particles (SiO<sub>2</sub>) to polyvinylidene fluoride (PVDF) casting solution on some properties of the resulting composite membranes was reported by Bottino et al.[33]. Increasing amounts of SiO<sub>2</sub> (ranging from 10 wt.% to 20 wt.%) added to more diluted 10 wt.% PVDF solutions yield membranes with permeate flux of 80 L/m<sup>2</sup>h to 400 L/m<sup>2</sup>h. Better retention of 45% was resulted by 3 g SiO<sub>2</sub> added to 100 g PVDF in N-methylpyrrolidone (NMP). These more relevant and beneficial effects due to the silica lies on the increase of the viscosity of the casting solutions that makes easier casting operations thus allowing the preparation of membranes not only with high mechanical properties but also with both better flux and retention.

### **2.1.2.5 Polymer membrane with addition of carbon nano-tubes**

Chemical and physical functionalization of multiwalled carbon nanotubes (MWCNT) has been commonly practiced to achieve better dispersion of carbon nanotubes (CNTs) in polymer matrix [11,46]. Carbon nanotubes are micro-meter graphene sheets rolled into a cylinder of nanoscale

diameter and capped with spherical fullerenes. CNTs have attracted much attention due to their extraordinary characteristics caused by their unique structure [47]. The CNTs have also been considered as ideal model sorbent system to investigate the effect of pore size and surface characteristics on the sorption and transport properties of the porous solids [48,49]. It has been reported experimentally that advanced water treatment could be applied by using ligned CNTs membranes, which produce nanoporous structure of membrane [48,50].

**Table 3**  
**Polymer/Inorganic Composite Membrane**

Polymer used	Method	Remark	Reference
PVDF/TiO <sub>2</sub>	Phase inversion method	TiO <sub>2</sub> loading increased hydrophilicity and fouling resistance of membrane. The maximum flux of 146 L/m <sup>2</sup> h was achieved with addition of TiO <sub>2</sub> of 1.95 wt.%.	[36]
PSf/PVP/TiO <sub>2</sub>	Phase inversion method with direct blended of TiO <sub>2</sub>	The membranes with addition of TiO <sub>2</sub> demonstrated an excellent anti-fouling performance (>90%) and particularly reducing the fouling resistance	[50]
PES/TiO <sub>2</sub>	Photocatalytic powder TiO <sub>2</sub>		[38]
PVDF/ZnO	Phase inversion method	The implantation of nano-ZnO into membrane inner surface demonstrated the enhancement of anti-irreversible fouling property. The water permeability of modified membrane almost doubled by adding 6.7% nano-ZnO to PVDF membrane.	[31]
PVDF/SPES/TiO <sub>2</sub>	Phase inversion method	The presence of 4wt.% TiO <sub>2</sub> in membrane structure demonstrated the increase of hydrophilicity, thus possess the dramatic photo-bactericidal effect on <i>Escherichia coli</i> ( <i>E.coli</i> )	[51]
PS/SiO <sub>2+</sub>	Phase inversion method	The effective pore radius of	[52]

PVDF/CNTs	Phase inversion method	<p>the membrane increased when the silica concentration in the casting solution is increased.</p> <p>The highly dispersion of CNTs in polyvinylidene fluoride occurred based on the immobilization the nanotubes in the pore structure. The importance of the size and uniformity of the nanotubes plays a big role in manufacturing processes for carbon nanotubes in polymeric matrices.</p>	[11]
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### 3.0 Summary

Membrane materials are currently the most important part in membrane technology and it was experiencing significant growth. Generally the development of membrane materials can be divided into two periods according to research activity: (i) the search for a suitable material (chemical composition) and membrane formation mechanism (1960s to late 1980s), and (ii) the evolution of more controlled conditions for membrane formulation to enhance membrane functionality and durability (late 1980s to date).<sup>1</sup> The selection of membrane material allows control over the nature and magnitude of the permeant-membrane physicochemical interaction. However, it would be beneficial if one could experimentally verify that the proper choice has been made prior to undertaking the often difficult tasks of membrane preparation and characterization. The objective of this chapter is to review the current development of membrane materials for ultrafiltration (UF), nanofiltration (NF) and reverse osmosis (RO) that is helpful to choose the suitable type of material.

Choice of membrane material, i.e. polymer, copolymer, inorganic, polymer/polymer, and polymer/inorganic, also determines the packing density and segment mobility of the materials chains, which comprise the solid regions of the membrane. This influences the mechanism of transport, membrane stability and membrane performance that often follows a common sense approach. The number of polymers has been studied in recent literatures and patents, which indicated that an ever-increasing number of polymers, copolymers and blends are being considered as potential membrane materials for liquid mixture separations. The application of polymeric material for a separation membrane depends of course upon both the throughput and the purity of the product transported through membrane. The most widely used polymers for commercial ultrafiltration (UF), nanofiltration (NF) and reverse osmosis (RO) membrane are polysulfone (PSf), polyethersulfone (PES), polyvinylidene fluoride (PVDF), polyetherimide (PEI), polyacrylonitrile (PAN), Cellulose Acetate (CA), polyamide (PA), polyfurane, polyether-polyfurane, polyvinylamine, polypyrrolidine, polypiperazine amide. Inorganic (nanoparticle) materials are used to membrane preparation as follows, titanium dioxide (TiO<sub>2</sub>), zinc oxide (ZnO) nano-particles, silica oxide (SiO<sub>2</sub>), alumina (Al<sub>2</sub>O<sub>3</sub>), and carbon nano-tubes (CNTs).

The emergence of nano-technology in membrane materials science could offer an attractive alternative to polymeric materials. Recent opinion in nano-technology is, that it deals with structures having at least one dimension that is sufficiently small, the order about one to several hundred nanometers. It is concerned with materials and systems, which have structures and components exhibit novel and significantly improved physical, chemical, and biological properties in order to exploit of novel phenomena and processes due to their nanoscale sized. There are a large number of nanofiltration membrane application made from a polymeric or an inorganic material for UF, NF and RO membranes. It is proposed that these novel materials represent the most likely opportunities for enhanced membrane filtration performance in a current trend and the future.

## Nomenclature

PSf	Polysulfone
PES	Polyethersulfone
PAN	Polyacrylonitrile
PS	Polystyrene
PC	Polycarbonate
PVDF	Polyvinylidene fluoride
PMMA	Polymethylmetacrylate
SPEEK	Sulfonated polyether-ether-ketone
PFSA	Perfluorosulfonic acid
PEI	Polyetherimide
SPEI	Sulfonated polyetherimide
SPC	Sulfonated polycarbonate
TiO <sub>2</sub>	Titanium oxide
ZnO	Zinc oxide
SiO <sub>2</sub>	Silica oxide
Al <sub>2</sub> O <sub>3</sub>	Alumina
UF	Ultrafiltration
NF	Nanofiltration
RO	Reverse osmosis
CNTs	Carbon nano-tubes

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